



**CATARAQUI BAY
WATER POLLUTION CONTROL PLANT
2025 ANNUAL REPORT**

**Environmental Compliance Approval Number: 2497-CYPPUP
Wastewater Collection System Owner: City of Kingston
Wastewater Treatment Facility Classification: Class IV**

TABLE OF CONTENTS

1 EXECUTIVE SUMMARY..... 3

2 PLANT DESCRIPTION AND TREATMENT PROCESS 3

2.1 SCREENING..... 3

2.2 GRIT REMOVAL 3

2.3 PRIMARY TREATMENT CHEMICAL FEED..... 3

2.4 FLOW SPLITTING..... 3

2.5 PRIMARY CLARIFIERS..... 4

2.6 BIOLOGICAL AERATED FILTERS..... 4

2.7 BACKWASH..... 4

2.8 DISINFECTION..... 4

2.9 DECHLORINATION SYSTEM..... 4

2.10 OUTFALL..... 5

2.11 SLUDGE DIGESTION..... 5

2.12 BIOSOLIDS DEWATERING 5

2.13 MISCELLANEOUS 5

Figure 1 – Cataraqui Bay Water Pollution Control Plant General Layout..... 6

3 OPERATION..... 8

4 PLANT PERFORMANCE 8

5 BIO-SOLIDS MANAGEMENT 9

6 MAINTENANCE 9

7 CAPITAL WORKS 10

8 EQUIPMENT CALIBRATIONS 10

9 COMPLAINTS..... 10

10 BYPASS AND SPILL SUMMARY 10

11 BYPASS RESULT INTERPRETATIONS..... 10

12 BIOSOLIDS RECIPIENTS 11

Table 1 – Biosolids Recipients 11

13 EFFLUENT OBJECTIVES AND LIMITS..... 11

Table 2 – Effluent Objectives and Limits..... 11

14 PLANT PERFORMANCE RESULTS 11

Table 3 – Raw Influent Results..... 11

Table 4 – Monthly Effluent Concentrations (Part 1) 12

Table 5 – Monthly Effluent Concentrations (Part 2) 12

Table 6 – Monthly Flows 12

Table 7 – Annual Plant Flows..... 13

15 NOTICE OF MODIFICATIONS TO SEWAGE WORKS..... 13

Figure 2 – Notice of Modification to Sewage Works 13

1 EXECUTIVE SUMMARY

Cataraqui Bay Water Pollution Control Plant (WPCP) operates under Ministry of the Environment, Conservation and Parks, Environmental Compliance Approval (ECA) number 2497-CYPPUP, issued to the owner, the Corporation of the City of Kingston. This report is to satisfy the requirements outlined in condition 11 of the aforementioned ECA. The facility was compliant with all conditions outlined in condition 7 of the above-mentioned ECA during 2025.

The sewage works has a rated capacity for an average daily flow of 55,000 m³/d, and a peak daily flow of 141,600 m³/d. The average daily raw influent flow into the plant was 25,483 m³/d, the maximum daily flow into the plant was 74,650 m³/d, and the total flow received by the plant was 9,317,209.06 m³ in 2025.

There were no bypass events at Cataraqui Bay WPCP.

There was a spill of digested sludge from a digester, and two spills of unburnt digester gas in 2025.

Planned and reactive maintenance as well as planned and unplanned capital works at the facility were undertaken throughout the year.

2 PLANT DESCRIPTION AND TREATMENT PROCESS

The following is a process overview and description of the treatment steps taken at the Cataraqui Bay WPCP.

2.1 SCREENING

The first step in the treatment process is screening, where large particles and floating debris such as wood, rags and plastics are removed from the raw wastewater. There are two active 6 mm diameter perforated plate fine screens each in a 2 m wide channel. Screenings are conveyed to a common wash/compactor prior to being discharged in a screening disposal bin. A coarse bar screen is located in a third manual bypass channel, as well as a fourth channel containing an overflow weir (hydraulic bypass of the screens) for emergency purposes only.

2.2 GRIT REMOVAL

The second step of preliminary treatment is grit removal. During this process, heavier solids in the wastewater settle, while the organics that require treatment stay in suspension and move on to the next step of the treatment process. The system is made up of two vortex grit removal tanks equipped with a paddle mixer, and a slurry pump in each tank. The grit is pumped to two grit classifiers used to de-water the grit slurry and discharge the grit into grit disposal bins.

2.3 PRIMARY TREATMENT CHEMICAL FEED

Immediately after the grit vortex tanks, the coagulant Ferric Chloride is added to the stream of wastewater. Chemically assisted coagulation is used to improve the removal of Phosphorous and Suspended Solids in the wastewater. Two chemical storage tanks feed two chemical feed pumps used to dose Ferric Chloride paced to the flow of liquid.

2.4 FLOW SPLITTING

The screened and de-gritted wastewater discharges into a channel where the flow is divided into two parshall flume flow meter channels. The flow is then split into a primary inlet channel leading to four identical primary clarifiers. Centrifugal blowers provide aeration to the primary influent channel to prevent settling in the channels.

2.5 PRIMARY CLARIFIERS

Four primary clarifiers make up the primary treatment system. Heavier organics settle by gravity to the bottom of the primary clarifiers. This forms a sludge blanket on the bottom of the tank. The settled sludge is collected by collector flights and scraped into a hopper at the end of the tank. Floating scum and grease is removed by surface skimmers located near the end of each clarifier. The settled sludge, and scum and grease, is then pumped to digestion facilities for further treatment.

2.6 BIOLOGICAL AERATED FILTERS

Primary effluent flows down a channel to a Primary Effluent Pumping Station (PEPS) composed of two wet wells and four submersible pumps. Primary effluent is pumped to the Biological Aerated Filter (BAF) Influent Channel. A supplemental alkalinity feed system is required to ensure adequate nitrification while maintaining an acceptable pH in the BAF effluent water. The alkalinity feed system is made up of four storage tanks, and two chemical feed pumps, and is dosed just after the discharge from the PEPS. The BAF is made up of six available cells with a common influent channel which then runs down to the bottom of each cell and filters upwards through two unique sets of media. The two types of media are: polystyrene beads, and K5 hard plastic honeycomb disks. The media is held in place below the top deck of the filter with nozzles which let filtered water out and hold the floating media in. In the filter the wastewater is aerated, this encourages growth of microorganisms which consume carbon dissolved in the wastewater, as well as reducing ammonia and phosphorus. The media is meant to provide a location for microorganisms, referred to as biomass, to grow, the media also helps to filter any suspended materials.

2.7 BACKWASH

The Biological Aerated Filters require regular backwashes to remove excess biomass from the media. Backwash residuals from the filters flows into two backwash residual tanks for temporary storage of the backwash water. The facility has the option to either co-thicken the backwash residuals by adding the backwash water to the primary inlet channel, or to feed the backwash residuals to two gravity thickeners. Alum is added to the backwash water as it is pumped out of the backwash residual tanks. The gravity thickeners are two clarifiers designed to allow solids to settle out and allow the supernatant to flow back and mix with the primary effluent ahead of the primary effluent pumping station. The solids from the gravity thickeners are pumped to a sludge thickening facility. The sludge thickening facility consists of two rectangular holding tanks, two Rotating Drum Thickeners (RDT's), and a polymer system. The thickening system increases the solids concentration of the residuals prior to being pumped to the primary digester. The filtrate from the RDT's is pumped back to the primary inlet channel.

2.8 DISINFECTION

Effluent from the BAF facility flows through a parshall flume to calculate the flow of water into the chlorine contact tank. A chlorine gas system provides chlorine for disinfection prior to entering the chlorine contact tank. The chlorine system is composed of two sets of large and small chlorinators dosing a chlorinated water solution to the BAF effluent stream. Two chlorine contact tanks provide contact time to adequately disinfect the effluent water.

2.9 DECHLORINATION SYSTEM

An effluent dechlorination system using Calcium Thiosulphate removes chlorine from the water prior to discharge into Lake Ontario. The system is made up of two metering pumps, and one chemical

storage tank. The Calcium Thiosulphate is dosed into the effluent in the outfall chamber immediately after the final effluent flow meter.

2.10 OUTFALL

After de-chlorination, the disinfected effluent from the chlorine contact tank is discharged back to Lake Ontario through a 1500 mm and a 900 mm outfall. 17 diffusers are installed at the end of each of the outfall pipes and are located 25 m offshore and 16 m below water surface level.

2.11 SLUDGE DIGESTION

Raw sludge, grease and scum, and thickened backwash residuals are pumped to the primary digester in regular intervals throughout the day. The sludge digestion facilities are composed of two anaerobic digesters with an interconnected digester gas system, one digested sludge holding tank, transfer, and mixing pumps, and a heat exchanger. Inside the digesters, the mixture is heated to approximately 36 °C to allow microorganisms to grow and consume carbon, producing methane gas and carbon dioxide. The digesters use recirculated digester gas and sludge, which has been heated through the heat exchanger, for mixing and to maintain optimal temperatures. The anaerobic digestion process produces gas and biosolids. The gas produced is rich in methane, which is used as fuel for the boiler system which in turn provides heat for the digestion process, and buildings within the facility. The biosolids produced through sludge digestion are dewatered and used on agricultural lands as a nutrient and soil conditioner when weather and crop conditions permit.

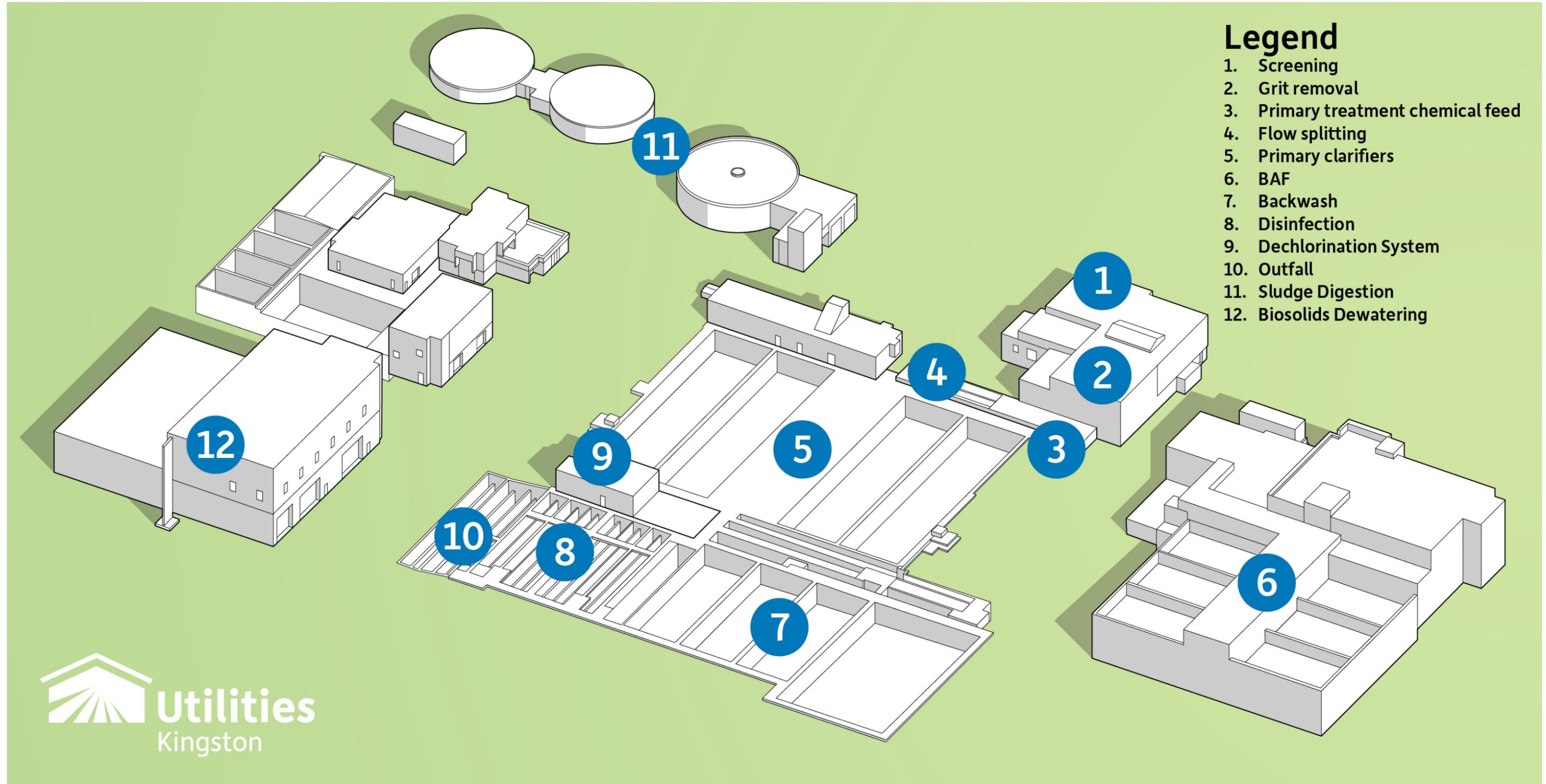
2.12 BIOSOLIDS DEWATERING

The dewatering facility is made up of two sludge feed pumps, a polymer preparation and feed system, two centrifuges with a capacity of dewatering 50 m³/hour, two screw conveyors, two biosolids storage bunkers, a centrate pumping station, two centrate equalization tanks with two centrate pumps. Liquid biosolids, which are about 1.5-2% solids, are pumped from the holding tank into 2 centrifuges. Polymer is added to the biosolids before it enters the centrifuge, this helps the solids stick together, aiding the dewatering process. The centrifuge spins at a high-speed, forcing solids to the outer drum. This separates the solids, referred to as cake, from the liquid, called centrate. The cake, which now has a solids content of about 24%, is conveyed to a shoot and dropped into the storage bunkers. The centrate, which contains many nutrients and some microorganisms, is returned to the headworks for treatment.

2.13 MISCELLANEOUS

The Cataraqui Bay WPCP has miscellaneous infrastructure required to support continued effective treatment of incoming Wastewater. This includes many controls, electrical power equipment, instrumentation, boilers, and emergency power generation for the entire facility.

Figure 1 – Cataraqi Bay Water Pollution Control Plant General Layout



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3 OPERATION

Adequate staffing as well as preventative maintenance, and regular equipment inspections resulted in minimal disruptions to the operation of the plant. Non flushable materials such as wipes, and grease continue to be prominent in the sewer system resulting in operational and maintenance challenges. Utilities Kingston continues to implement a public education program to educate customers and bring awareness to types of materials that should not be flushed down drains and toilets, and then into the sewers. This program included radio and newspaper campaigns, social media campaigns, bill stuffers, information on back of parking tickets, and bus information signs. This has been an ongoing campaign for many years with positive results.

The pilot headworks polymer system continued through 2025 to investigate the effectiveness of the system through each of the four seasons, see Figure 2 for the Notice of Modification to Sewage Works. This polymer system was implemented as a response to the operational difficulties and increased effluent concentrations experienced in 2023. The system has been online since May 2024, and operators have noted improved effluent concentrations during this time. Laboratory data and observations have been monitored closely during the pilot period. A permanent polymer system has been budgeted for 2026.

Operational challenges of significance experienced in 2025 are listed below:

In May 2025, Digester 2 had an entry hatch fail at the base of the digester. This resulted in the uncontrolled draining of the entire digester. Upon discovery of the spill and associated failure of the hatch, staff set up an emergency pumping system to pump the incoming sludge out of the hatch area and into the holding tank beside the digester. This limited the volume of spilled sludge to 56 m³. Following this event, the digester was cleaned and prepped for work to bring the digester back online. The wash water from the cleanout process was returned to the head of the primary clarifiers which greatly increased the concentration of Total Suspended Solids (TSS) received by the primary clarifiers, and resulted in elevated TSS in the plant effluent. The gas production in the remaining digester dropped following this process, likely due to the introduction of old biomass from the cleanout as well as reduced digestion with digester 2 offline. The issues were addressed with ongoing, careful monitoring of chemical dosages, and proactive maintenance on the digester gas system.

Following maintenance on the nozzle deck of BAF cell number 4, biomass was re-established in the cell which ensured adequate nitrification could be achieved when the cell was brought back online. The efforts resulted in minimal impacts to the treatment process and final effluent quality upon startup.

Through the summer and fall of 2025, Cataraqui Bay WPCP experienced extremely low influent flows. Operators made many process adjustments including taking two primary clarifiers offline, and reducing backwash frequencies to ensure plant effluent met the required limits.

The digester gas flare stack continued to encounter operational difficulties during high wind weather events. Staff proactively redistribute gas usage throughout the plant to ensure the flare stack receives a strong flow of gas and remains lit during these weather events. The facility did not see any digester gas spills from the flare stack in 2025.

4 PLANT PERFORMANCE

The ECA number 2497-CYPPUP lists the limits and objectives for the concentrations of certain effluent parameters, this is shown in Table 2. The effluent objectives listed in this table are the concentrations Utilities Kingston are expected to be below. The effluent concentration limits listed in the table are the concentrations Utilities Kingston are required to be below. The Cataraqui Bay WPCP

was compliant with all monthly average effluent limits. The 2025 monthly average effluent monitoring results can be found on Tables 4 and 5.

The plant exceeded the average monthly concentration objective of TSS, Total Phosphorous (TP), and the E. Coli parameters once each, in different months through 2025 (Tables 4 and 5). Operational adjustments were made and each of those objective exceedances were corrected for the following month.

The tables below include several parameters that are monitored to satisfy ECA requirements, even though they do not have limits or objectives assigned to them. These metrics are essential for operational oversight and process control. This includes Nitrate Nitrogen which is produced during nitrification of Total Ammonia Nitrogen. Higher Nitrate Nitrogen concentrations are an indicator of complete nitrification occurring within the plant.

The chlorine residual in the final effluent did not exceed the monthly average limit of 0.04 mg/L for any month of the year.

No other parameters were above their limit or objective.

The treatment process is monitored through in-house laboratory work on a regular basis throughout each week. This allows operations staff to react to any issues quickly and effectively.

The concentration of raw influent into the plant remains consistent throughout the year, however during the wet seasons concentrations are somewhat reduced. This increase indicates some infiltration of ground water, or potentially illegal sump pump connections to the sanitary collection system. Annual raw influent monitoring results can be seen in Table 3. Raw Influent, and Final Effluent samples were collected and submitted to a third-party laboratory at or above the required frequencies based on the ECA. The average daily flow into the treatment plant was 46.3% of the design capacity (55,000 m³/day). Table 8 shows the average annual plant flows for the past 7 years. The monthly flows as well as the peak daily flow from each month are displayed in Table 6.

5 BIO-SOLIDS MANAGEMENT

Cataraqui Bay WPCP processed 57,904 m³ of liquid sludge through the centrifuge. Approximately 2,988 Metric Tonnes of sludge cake was stored on site until GFL Environmental, contractor hired by Utilities Kingston, hauled the material off-site for land application.

The location and date of land application of the bio-solids produced largely depends on weather, and the crops being grown on the receiving lands. Table 1 contains the Non-Agricultural Source Materials (NASM) Plan numbers and addresses of receiving lands for bio-solids produced by the City of Kingston.

6 MAINTENANCE

Staff continue to follow a preventative maintenance program in accordance with the manufacturer's recommendations.

Additional Maintenance completed this year:

- Infrared scans of HV electrical were performed across the plant.
- Equipment and motors had routine vibration monitoring conducted.
- The onsite diesel generator was serviced and received routine maintenance.
- Two new influent pH probes installed.
- Inspection of BAF Cell 4 nozzle deck, and replacement of broken nozzles.
- Heat trace installed on scum pump discharges.
- Primary clarifier tanks 1, 3, and 4 inspections and repairs.
- Installation of a new primary digester heat exchanger.

- The drive end bearing was replaced on a centrifuge.
- A new chlorine regulator for chlorine gas system was installed.
- Completed all digester gas system equipment inspections and testing in accordance with Technical Standards and Safety Authority (TSSA) requirements.

7 CAPITAL WORKS

Capital works on the Catarauqui Bay WPCP in 2025 include:

- Digester 2 cleanout, roof rehab, and inspection.
- New refrigerant dryer installed for BAF compressor system.
- One of the primary effluent pumps was rebuilt.
- BAF blower 3 was serviced and rebuilt.
- Purchase of emergency standby 6" portable pump.
- Motor Control Centre (MCC) and Programmable Logic Controller (PLC) battery replacements.
- A failed centrate mixer was replaced.

8 EQUIPMENT CALIBRATIONS

Third party contractors calibrated all plant flow meters, online analyzers, and lab equipment. As a result, the facility saw limited downtime of major equipment and saw very few mechanical or electrical failures this year. Calibration records are available upon request.

9 COMPLAINTS

In the 2025 reporting year, the Catarauqui Bay WPCP received no official complaints regarding the facility or treatment process.

10 BYPASS AND SPILL SUMMARY

There were no secondary treatment bypasses at the Catarauqui Bay WPCP in 2025.

The failure of an entryway hatch resulted in the spill of 56 m³ of liquid sludge from Digester 2. The spill was contained and a contractor was hired to clean up the spilled sludge and restore the surrounding area. Digester 2 remains offline and Utilities Kingston has begun the process of rehabilitating the digester to put it back into service. In addition to the spill of liquid sludge, during the same event there was a spill of unburnt digester gas.

There were two spill events of unburnt digester gas to the environment totaling 360 m³. Both spills were reported to the MECP. One as detailed above occurred that the same time as the spill of liquid sludge from Digester 2, and the other release was experienced during a routine maintenance procedure. Condensation was being released from the gas system, and a drain valve was left open, which led to the release of digester gas. The leak was identified and the valve was closed within 1 hour.

11 BYPASS RESULT INTERPRETATIONS

As noted above there were no bypasses at the Catarauqui Bay WPCP in 2025. However, it should be noted that bypass discharges have a high bacteria count due to the lack of disinfection. CBOD₅, TP, and TSS results are typical raw sewage influent levels. When bypasses occur, best efforts are made to capture the debris contained in any discharges to the lake. After each bypass event, shoreline inspections near discharge points are done to monitor any debris that may come ashore, and clean-up is done if debris is found.

For further information about this report or any questions regarding accessibility, contact Tim Bourne at tbourne@utilitieskingston.com or call 613-546-1181 Ext 2190.

12 BIOSOLIDS RECIPIENTS

Table 1 – Biosolids Recipients

Non-Agricultural Source Materials (NASM) Plan	Address
60616	Lot 13-14 Concession 2 Town of Greater Napanee
60616	Lot 13 Concession 3 Town of Greater Napanee
25209	Lot 50 Concession 4 Stone Mills Township
60611	Lot 37-38 Concession 4 Stone Mills Township

13 EFFLUENT OBJECTIVES AND LIMITS

Table 2 – Effluent Objectives and Limits

Effluent Parameter	Objective	Limits
CBOD5	15.00 mg/L (Monthly Average)	25.00 mg/L (Monthly Average)
Total Suspended Solids	15.00 mg/L (Monthly Average)	25.00 mg/L (Monthly Average)
Total Phosphorus	0.80 mg/L (Monthly Average)	1.00 mg/L (Monthly Average)
Total Ammonia Nitrogen (TAN) Summer (June 1 to November 30)	6.0 mg/L	8.0 mg/L
Total Ammonia Nitrogen (TAN) Winter (December 1 - May 31)	12.0 mg/L	15.0 mg/L
Total Chorine Residual	Non Detectable	0.04 mg/L
E. Coli	100 CFU/100mL	200 CFU/100mL
pH	6.5 - 8.5	6.0 - 9.0

14 PLANT PERFORMANCE RESULTS

Table 3 – Raw Influent Results

(Monthly Average)

Month	BOD5 (mg/L)	Total Suspended Solids (mg/L)	Total Phosphorus (mg/L)	Total Ammonia Nitrogen (mg/L)	Total Kjeldahl Nitrogen (mg/L)	pH
January	234.00	140.00	3.20	23.54	37.74	7.32
February	232.00	219.00	4.00	28.25	43.60	7.33
March	229.00	226.00	4.10	17.50	30.35	7.31
April	144.00	139.00	2.50	16.23	26.00	7.52
May	141.00	139.00	3.10	15.60	28.13	7.45
June	149.00	156.00	3.60	20.53	33.15	7.33
July	233.00	368.00	7.90	25.80	50.50	7.21
August	227.00	238.00	4.70	26.98	48.28	6.98
September	247.00	225.00	4.40	26.90	47.13	7.15
October	241.00	215.00	5.40	29.72	50.88	7.25
November	173.00	254.00	3.60	18.28	33.25	7.38
December	172.00	189.00	3.30	17.94	31.52	7.49
Annual Average	201.83	209.00	4.15	22.27	38.38	7.31

Table 4 – Monthly Effluent Concentrations (Part 1)

(Monthly Average)

Month	CBOD5 (mg/L)	Total Suspended Solids (mg/L)	Total Phosphorous (mg/L)	Total Ammonia Nitrogen (mg/L)	Total Kjeldahl Nitrogen (mg/L)
January	5.00	11.80	0.57	6.15	7.84
February	8.00	22.80*	0.77	7.43	11.38
March	2.80	7.00	0.31	1.03	3.05
April	2.10	6.40	0.36	1.80	3.54
May	2.10	5.90	0.53	0.87	2.65
June	1.90	6.80	0.62	1.59	3.10
July	2.00	4.20	0.58	1.54	3.78
August	5.30	14.80	0.90*	6.88	9.35
September	2.60	10.00	0.57	3.38	5.80
October	4.30	13.00	0.71	3.53	7.82
November	3.00	6.50	0.52	1.72	3.73
December	2.90	8.40	0.61	1.78	3.72
Annual Average	3.50	9.80	0.59	3.14	5.48

*Indicates an exceedance of the Monthly Average Effluent Concentration objective

Table 5 – Monthly Effluent Concentrations (Part 2)

(Monthly Average)

Month	Nitrate	Nitrite	E. Coli	pH	Total Residual Chlorine (mg/L)	Acute Lethality (Pass or Fail)
January	22.46	0.15	4	7.29	0.01	PASS
February	20.03	0.11	12	7.25	0.01	N/A
March	17.63	0.04	11	7.35	0.01	N/A
April	18.42	0.21	18	7.42	0.00	PASS
May	18.83	0.20	17	7.31	0.01	N/A
June	20.45	0.32	16	7.32	0.01	N/A
July	26.02	0.29	13	7.18	0.01	PASS
August	25.40	0.33	72	7.23	0.01	N/A
September	28.28	0.51	15	7.43	0.01	N/A
October	26.16	0.48	16	7.41	0.01	PASS
November	21.33	0.24	23	7.50	0.01	N/A
December	16.28	0.38	111*	7.28	0.01	N/A
Annual Average	21.77	0.27	27	7.33	0.01	N/A

*Indicates an exceedance of the Monthly Average Effluent Concentration objective

Table 6 – Monthly Flows

Month	Rated Capacity (m3/day)	Average Flow (m3/day)	Approved Peak Flow (m3/day)	Peak Flow (m3/day)
January	55,000	23,362	141,600	37,191
February	55,000	19,016	141,600	21,792
March	55,000	37,812	141,600	74,650
April	55,000	33,618	141,600	62,996
May	55,000	32,724	141,600	61,228
June	55,000	26,050	141,600	35,580
July	55,000	20,141	141,600	26,574
August	55,000	18,407	141,600	21,595
September	55,000	18,334	141,600	20,055
October	55,000	20,451	141,600	37,067
November	55,000	26,487	141,600	37,498
December	55,000	28,855	141,600	58,011

Table 7 – Annual Plant Flows

Parameter	2019	2020	2021	2022	2023	2024	2025
Average (m3/day)	29,251	27,189	27,225	29,381	28,707	25,890	25,483
Max (m3/day)	91,976	82,297	51,566	88,225	108,514	80,178	74,650
Design (m3/day)	38,800	38,800	38,800	38,800	38,800	55,000	55,000
Design Peak (m3/day)	134,400	134,400	134,400	134,400	134,400	141,600	141,600
Daily/Design (%)	75.4	70.1	70.2	75.7	74.0	47.1	46.3
Max/Peak (%)	68.4	61.2	38.4	65.6	80.7	56.6	52.7

15 NOTICE OF MODIFICATIONS TO SEWAGE WORKS

Figure 2 – Notice of Modification to Sewage Works



Notice of Modification to Sewage Works

RETAIN COPY OF COMPLETED FORM AS PART OF THE ECA AND SEND A COPY TO THE WATER SUPERVISOR (FOR MUNICIPAL) OR DISTRICT MANAGER (FOR NON-MUNICIPAL SYSTEMS)

Part 1 – Environmental Compliance Approval (ECA) with Limited Operational Flexibility <i>(Insert the ECA's owner, number and issuance date and notice number, which should start with "01" and consecutive numbers thereafter)</i>		
ECA Number 2497-CYPPUP	Issuance Date (mm/dd/yy) 12/22/2023	Notice number (if applicable)
ECA Owner The Corporation of the City of Kingston	Municipality Kingston	

Part 2: Description of the modifications as part of the Limited Operational Flexibility <i>(Attach a detailed description of the sewage works)</i>
<p>Implementation of 3 trials to add polymer to improve the performances of the primary clarifiers and BAF.</p> <p>A description of the trials is provided in the attached Trial Proposal Report from Northland</p> <p>Chemical dated January 8, 2024. The performance of the plant for each of the trials will be evaluated.</p> <p>Description shall include:</p> <ol style="list-style-type: none"> A detail description of the modifications and/or operations to the sewage works (e.g. sewage work component, location, size, equipment type/model, material, process name, etc.) Confirmation that the anticipated environmental effects are negligible. List of updated versions of, or amendments to, all relevant technical documents that are affected by the modifications as applicable, i.e. submission of documentation is not required, but the listing of updated documents is (design brief, drawings, emergency plan, etc.)

Part 3 – Declaration by Professional Engineer						
<p>I hereby declare that I have verified the scope and technical aspects of this modification and confirm that the design:</p> <ol style="list-style-type: none"> Has been prepared or reviewed by a Professional Engineer who is licensed to practice in the Province of Ontario; Has been designed in accordance with the Limited Operational Flexibility as described in the ECA; Has been designed consistent with Ministry's Design Guidelines, adhering to engineering standards, industry's best management practices, and demonstrating ongoing compliance with s. 53 of the Ontario Water Resources Act; and other appropriate regulations. <p>I hereby declare that to the best of my knowledge, information and belief the information contained in this form is complete and accurate</p>						
<table border="0"> <tr> <td>Name (Print) James K Steele</td> <td>PEO License Number 100067361</td> </tr> <tr> <td>Signature <i>James K Steele</i></td> <td>Date (mm/dd/yy) 03/04/24</td> </tr> <tr> <td>Name of Employer J.L. Richards & Associates Limited</td> <td></td> </tr> </table>	Name (Print) James K Steele	PEO License Number 100067361	Signature <i>James K Steele</i>	Date (mm/dd/yy) 03/04/24	Name of Employer J.L. Richards & Associates Limited	
Name (Print) James K Steele	PEO License Number 100067361					
Signature <i>James K Steele</i>	Date (mm/dd/yy) 03/04/24					
Name of Employer J.L. Richards & Associates Limited						

Part 4 – Declaration by Owner				
<p>I hereby declare that:</p> <ol style="list-style-type: none"> I am authorized by the Owner to complete this Declaration; The Owner consents to the modification; and This modifications to the sewage works are proposed in accordance with the Limited Operational Flexibility as described in the ECA. The Owner has fulfilled all applicable requirements of the <i>Environmental Assessment Act</i>. <p>I hereby declare that to the best of my knowledge, information and belief the information contained in this form is complete and accurate</p>				
<table border="0"> <tr> <td>Name of Owner Representative (Print) Heather Roberts</td> <td>Owner representative's title (Print) Director, Water & Wastewater Services</td> </tr> <tr> <td>Owner Representative's Signature <i>Heather Roberts</i></td> <td>Date (mm/dd/yy) 04/04/24</td> </tr> </table>	Name of Owner Representative (Print) Heather Roberts	Owner representative's title (Print) Director, Water & Wastewater Services	Owner Representative's Signature <i>Heather Roberts</i>	Date (mm/dd/yy) 04/04/24
Name of Owner Representative (Print) Heather Roberts	Owner representative's title (Print) Director, Water & Wastewater Services			
Owner Representative's Signature <i>Heather Roberts</i>	Date (mm/dd/yy) 04/04/24			

EAB Form December 2, 2013